

**Amendments to the Claims:**

This listing of claims will replace all prior versions, and listings, of claims in the application:

**Listing of Claims:**

1. (Currently Amended) A process for the production of an olefin oxide, which process comprises the steps of:

reacting a feed comprising an olefin and oxygen in the presence of a silver-containing catalyst, wherein before the catalyst has reached an advanced stage of ageing, reaction conditions comprise a reaction temperature above 255 °C and an olefin content of the feed in the range of from above 25 mole-% to at most 80 mole-%, relative to the total feed; and

maintaining the reaction conditions for at least a period of time which is sufficient to effect a cumulative olefin oxide production of at least 1000 kmole of olefin oxide per m<sup>3</sup> catalyst bed before the catalyst has reached an advanced stage of ageing.

2. (Original) A process as claimed in claim 1, wherein the olefin is ethylene.
3. (Original) A process as claimed in claim 1, wherein the olefin content of the feed is in the range of from 30 to 80 mole-%.
4. (Original) A process as claimed in claim 3, wherein the olefin content of the feed is in the range of from 35 to 70 mole-%.
5. (Currently Amended) A process as claimed in claim 1, wherein the olefin content of the feed is maintained at the value as defined for at least a period of time which is sufficient to effect an olefin oxide production of at least 5000 kmole of olefin oxide per m<sup>3</sup> catalyst bed before the catalyst has reached an advanced stage of ageing.
6. (Original) A process as claimed in claim 1, wherein the reaction temperature is in the range of from 260 to 325 °C.
7. (Original) A process as claimed in claim 6, wherein the reaction temperature is in the range of from 270 to 310 °C.
8. (Currently Amended) A process as claimed in claim 1, wherein the reaction temperature is maintained at the value as defined for at least a period of time which is sufficient to effect an olefin oxide production of at least 5000 kmole of olefin oxide per m<sup>3</sup> catalyst bed before the catalyst has reached an advanced stage of ageing.

9. (Original) A process as claimed in claim 1, wherein “an advanced stage of ageing” of the catalyst is defined by a cumulative olefin oxide production of at least 10,000 kmole of olefin oxide per m<sup>3</sup> of catalyst bed.

10. (Original) A process as claimed in claim 1, wherein “an advanced stage of ageing” of the catalyst is defined by a cumulative olefin oxide production of at least 2000 kmole of olefin oxide per m<sup>3</sup> of catalyst bed.

11. (Canceled)

12. (Original) A process as claimed in claim 1, wherein the catalyst comprises, in addition to silver, rhenium or compound thereof, and a rhenium co-promoter selected from tungsten, molybdenum, chromium, sulfur, phosphorus, boron, and compounds thereof.

13- 22. (Canceled)

23. (Original) A method of using an olefin oxide for making a 1,2-diol, a 1,2-diol ether or an alkanolamine comprising converting the olefin oxide into the 1,2-diol, the 1,2-diol ether or the alkanolamine, wherein the olefin oxide has been obtained by a process as claimed in claim 1.

24. (Previously Presented) A process as claimed in claim 1, additionally comprising maintaining a reaction temperature of at most 325 °C and an olefin content of the feed of at most 80 mole-%, relative to the total feed, after the catalyst has reached an advanced stage of ageing.